Ultrasound Assisted Synthesis of Diethyl-2,2’-Thiodiacetate with 2-Bromoethylacetate Under a New Polymer-Supported Phase-Transfer Catalyst in Solid-Liquid Condition

Rajendran V* and Harikumar K2

1Head of The Department of Chemistry, Pachaiyappa’s College for Men, Kanchipuram, TamilNadu, India-631 501
2Sri Chandrashekarendra Saraswathi Viswa Mahavidyalaya, Kanchipuram, Enathur, Tamil Nadu, India-631 561

Abstract

In this work, a new polystyrene-bound single-onium phase-transfer catalyst was synthesized, and their catalytic activities were investigated in the synthesis of diethyl-2,2’-thiodiacetate derivatives of thioether. The new insoluble polymer anchored mono-site phase-transfer catalyst showed significant high catalytic activity as compared to soluble single site phase-transfer catalysts. The comparative kinetic investigation reveals that the diethyl-2,2’-thiodiacetate of ethyl-2-bromoacetate is faster than sodium sulfide in the presence of the new catalyst. This catalyst can be used several times with consistent catalytic activity. Experimental observations support an interfacial-type mechanism.

Keywords: Phase-transfer catalysis; Polymer-supported phase-transfer catalyst; Ultrasound irradiation; Ethyl-2-bromoacetate; Solid-liquid reaction; Kinetics.

Introduction

Currently, phase-transfer catalysis (PTC) is a key green approach [1] for driving reactions involving immiscible reactants [2-6]. However, application of this methodology to organic reactions has encountered two major problems viz: (i) the recovery and reuse of the catalyst and (ii) the separation and purification of the final product [7,8]. To circumvent the predicament of separation of catalyst from the reaction mixture, for the first time Regen [9] reported anchoring the phase-transfer catalysts to a polymer backbone and suggested the name “Triphase Catalysis”. Organic reactions catalyzed by triphase catalysts [10-13] have created remarkable attention for its application in synthesis of organic compounds. The vital considerations in the selection of the catalyst are economy of scale and efficiency of the PTC, particularly on the explicit industrial scale preparation of organic compounds. To cater these requirements, multi-site phase-transfer catalysts (MPTC) have been developed and revealed more efficient in activity than conventional single-site phase-transfer catalysts [14-18], and these catalysts are successfully employed for the generation of dihalocyclopropanes [19], which are generally prepared traditionally with lot of predicaments [20]. Synthesis of polymer-supported multi-site phase-transfer catalysts (PS-MPTC) of the ammonium type have not been explored much in contrast to the soluble multi-site PTCs. However, the demand and requirement of these triphase catalysts are on the rise due to their popularity.

Thioethers, which have been widely employed as perfume additives [21] and inverse phase-transfer catalysts [22,23] are generally synthesized in a homogeneous reaction [24]. Phase-transfer catalysis (PTC) is well-recognized as an invaluable methodology in organic synthesis in recent years [25-27]. The advantages of the PTC method for synthesizing thioethers are increased reaction rate and selectivity, hydrophilic conditions and low energy requirement. Searching for a more effective condition to enhance the reaction or to elevate the conversion is the primary purpose in phase-transfer catalysis in combined with ultrasonic waves [28-33]. Inventing selective, efficient and eco-friendly methods for applications in complex organic synthetic manipulations constitutes a major chemical research effort. In this regard, several non-conventional methods are emerging that involve reactions in aqueous media [34,35] or those that are accelerated by exposure to microwave [36-38] or ultrasound [39-44] irradiation. These methods are now recognized as viable environmentally benign alternatives. Although, sonication methods have been initially applied to homogeneous reactions in a variety of solvents, this approach has now evolved into a useful technique in heterogeneous reactions. A vast majority of sonochemical applications in the synthesis deal with reactions involving metals [43-52] organic phase insoluble reagents, or their aqueous solutions [53-76]. Our interest was centered on first time evaluating the influence of ultrasound in association with phase-transfer catalyst on the rate of alkyl thioether formation. This work investigates the substitution of alkyl bromides (RBr) to sodium sulfide (Na₂S), including linear and branched alkyl groups and the application of phase-transfer catalysts in combination with ultrasound obviously provides a more efficient synthetic approach for the preparation of thioethers. These PSPTC reactions were carried out in a soild-liquid two-phase medium. In the absence of a phase-transfer catalyst and ultrasound, less than 5% conversion was detected even after 4 h of reaction. In contrast high yields of products were obtained in shorter reaction time using 4 mol% (based on the amount of alkyl bromide) of the phase-transfer catalyst, polymer-supported benzyl N-ethyl-N-di-isopropyl ammonium chloride (PSPTC) and ultrasound 40 kHz (300 W) conditions. Kinetics of the substitution of ethyl-2-bromoacetate to sodium sulfide, including the effect of amount of catalyst, agitation speed, quaternary ammonium salts, amount of sodium hydroxide, organic solvents, temperature and ultrasound frequency on the conversion were investigated in detail.

*Corresponding author: Rajendran V, Head of The Department of Chemistry, Pachaiyappa’s College for Men, Kanchipuram, TamilNadu, India, Fax no: +91-44-27266824; Email: venugopal.rajendran@gmail.com

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With all these antecedents, we decided to synthesize a new monoactive site onium salt with two active sites viz., polymer-supported benzyl-N-ethyl-N-di-isopropyl ammonium chloride (PSPTC) by a facile method (Scheme 1). We investigated the catalytic efficiency of the new catalyst by following the comparative kinetics of thioether addition to sodium sulfide and ethyl-2-bromooacetate (EBA) under pseudo-first-order conditions (Scheme 2). Also, to the best of our knowledge, there is no systematic kinetic study of thioetherification addition to sodium sulfide involving polymer-supported monosite phase transfer catalysts. Kinetic investigation has been carried out by varying experimental parameters and from the obtained kinetic results, a plausible reaction mechanism has been proposed. Comparative catalytic efficiency of new onium salt and other onium salts (single-active site) were evaluated. (Schemes 3 and 4) shows the images of insoluble polymer-supported benzyl chloride and polymeric insoluble benzylethyldiisopropyl ammonium chloride (PSPTC).

**Experimental**

**Chemicals**

All the reagents, including, sodium sulfide (Merck), ethyl-2-bromooacetate (Merck), polymer-supported benzyl chloride (Aldrich), biphenyl (Aldrich), tetrabutylammonium chloride (TBAC) (CDH), tetrabutylammonium bromide (TBAB) (CDH), benzyltriethyl ammonium chloride (BTEAC) (CDH), tetrathyammonium chloride (TEAC) (CDH), tetrathyammonium bromide (TEAB) (CDH), potassium hydroxide (CDH), potassium carbonate (CDH), n-hexane (CDH), toluene (CDH), chlorobenzene (CDH), anisole (CDH), diethyl ether (CDH) and other reagents for synthesis were guaranteed grade (GR) chemicals and were used without further purification.

**Instrumentation**

$^1$H NMR and $^{13}$C spectra were recorded on a Bruker 300 MHz and 75 MHz respective using TMS as an internal standard. Gas chromatography was carried out using a GC-Varian 3700 model. Ultrasonic water bath, Equitron, Media Instrument Manufacturing Company, Chennai, India-600004. The ultrasonic generator was a thermostatic bath equipped with dual frequencies (28/40 kHz) and electric power 300 W with 0.0126 W/mL of power density.

**Ultrasonic process equipment**

Ultrasonic energy is transmitted to the process vessel through the liquid medium, usually water in the tank. For safety purpose, the sonochemical reactor consisted of two layers stainless steel body. The sonochemical reactor configuration used in the present work is basically an ultrasonic bath. The internal dimension of the ultrasonic cleaner tank is 48 cm $\times$ 28 cm $\times$ 20 cm with liquid holding capacity of 5 liters. Two types of frequencies of ultrasound were used in these experiments, which are 28 kHz and 40 kHz with each output as 300 W. Both ultrasounds separately produces through a flat transducer mounted at the bottom of the sonicator. The reactor was a 250 mL three-necked Pyrex round-bottom flask. This reaction vessel was supported at the centre of the ultrasonic cleaning bath 2 cm above from the position of the transducer to get the maximum ultrasound energy. All the experimental parameters were done at 40 kHz with output power of 300 W.

**Synthesis of a New PSPTC**

**Preparation of a new polymer-supported benzyl N-ethyl-N-di-isopropyl ammonium chloride (PSPTC)**

In the polymer-supported benzyl chloride (2 g) was swelled in acetonitrile (150 mL) for about 24 h and transferred into a 500 mL three-necked round bottomed flask with excess disopropylethylamine (20 mL). The reaction mixture was stirred continuously using a mechanical stirrer equipped with a poly (tetrafluoroethylene) (PTFE) half-moon blade agitating at 600 rpm under a nitrogen atmosphere. The reaction was carried out at reflux condition for 50 h. The solvent was then completely removed under vacuo and the onium salt viz., polymer-supported benzyl N-ethyl-N-di-isopropyl ammonium chloride (PSPTC) was washed with diethyl ether, methanol and acetone (Scheme 2) was stored in a CaCl$_2$ desiccator. The extent of quaternization, the amount of chloride ion present in the PSPTC was quantitatively estimated by Volhard’s method and found to be 1.1 mequiv$^1$.

FT-IR (KBr), cm$^{-1}$: 1152(C–N$^+$), 1443(C–O), 1605(aromatic C=C), 2931(alkyl stretching).

**Synthesis of Diethyl-2,2‘-Thiodiacetate under Mechanical Stirring**

Synthesis of diethyl-2,2‘-thiodiacetate under mechanical stirring. To the mixture of Na$_2$S (6 g, 77 mmol) in water (10 mL) and the
newly synthesized PSPTC (1.0 g), was added under overhead stirring to generate the sulphur anion. Then ethyl-2-bromo acetate (1.0 g, 6 mmol) in chlorobenzene (40 mL) was added slowly. The reaction mixture was heated at 60°C for 4 h with vigorous stirring. The crude product was isolated by simple extraction with diethyl ether (3 × 25 mL). The organic layer was collected and the solvent was evaporated under reduced pressure. The crude product was chromatographic (SiO₂) employing hexaneethyl acetate (9:1) as an eluant to obtain a pure monodervative. The identity of the product was confirmed by 1H NMR and 13C NMR spectra of the product. m.p.t. 306–308 °C. Yield: 88%; 1H NMR(400 MHz, CDCl₃); δ: 0.96–0.98 (t, 3H, CH₃), 5.34–1.33–1.45 (m, 2H, CH₂), 1.71–1.86 (m, 2H, CH₂), 3.90–4.01 (t, 3H, CH₃), 7.13, 8.18 (m, 4H, Ar–CH); 13C NMR (100 MHz, CDCl₃); δ: 14.12 (CH₃), 19.16 (CH₂), 32.01 (CH₂), 68.67 (CH₃), 115.31, 121.72, 140.05,163.64 (Ar–CH). 

Reaction Mechanism and Kinetic Model

The reaction was conducted in a 250 mL three-necked Pyrex round-bottom flask which permits agitating the solution, inserting the water condenser to recover organic reactant and taking samples and feeding the reactants. This reaction vessel was supported at the centre of the sonicator. Known quantities of chlorobenzene (30 mL, solvent), sodium sulfide powder (6 g in 10 mL water) and 0.2 g biphenyl (IS-internal standard) were introduced into the reactor. Then, 1.0 g of ethyl-2-bromo acetate (6 mmol) and 1.0 g of the newly synthesized PSPTC were introduced to the reactor to start the reaction. The reaction mixture was stirred at 300 rpm. The phase separation was almost immediate on arresting the stirring process. Samples were collected from the organic layer of the mixture (by stopping the stirring for 20-30 seconds each time) at regular time intervals. A pinch of anhydrous CaCl₂ was placed in the sample vials to absorb any moisture present in the organic layer. Each run consisted of six samples taken over the period ranging from 5 to 30 minutes. The kinetic was followed by estimating the concentration of ethyl-2-bromoacetate that disappeared and measured by a gas Chromatography (GC-Variian 3700 model). The analyzing conditions were as follows; Column, 30 m × 0.525 mm i.d. capillary column containing 100% poly(dimethyl siloxanen); injection temperature, 250°C; FID detector (300°C). Yields were determined from standard curve using biphenyl as an internal standard.

Definition

The conversion (X) of ethyl-2-bromo acetate (EBA) is defined as follows:

\[ X = 1 - \frac{[\text{EBA}_{\text{app}}]}{[\text{EBA}_{\text{in}}];} \]  

Where \([\text{EBA}_{\text{app}}]\) and \([\text{EBA}_{\text{in}}]\) represent the concentration of ethyl-2-bromo acetate in the organic phase at a given time (t) t=0 and t>0, respectively.

Rate expression

The rate expression for this reaction may be expressed as:

\[ -\frac{d[\text{EBA}_{\text{app}}]}{dt} = k_{\text{app}}[\text{EBA}_{\text{in}}]; \]  

Where \([\text{EBA}_{\text{in}}]\) is concentration of ethyl-2-bromoacetate in the organic phase and \(k_{\text{app}}\) is the apparent reaction rate constant. This reaction is carried out in a batch reactor, so the diminution rate of EBA with time (t) can be expressed as:

\[ d[\text{EBA}_{\text{app}}]/dt = -r_{\text{EBA}} = k_{\text{app}}[\text{EBA}_{\text{app}}]; \]  

On integrating the Eq. (3) yields:

\[ -\ln(1-X) = k_{\text{app}} x t \]  

Using Eq. (4), we can get the \(k_{\text{app}}\) value experimentally by plotting \(-\ln(1-X)\) against time, (t).

Results and Discussion

Effects of ultrasound and mechanical stirring on the reaction

To ascertain the influence of agitation speed on the rate of thioeifiercation of sodium sulfide, the speed of agitation was varied in the range of 0-500 rpm along with ultrasound irradiation (40 kHz, 300 W) using polymer-supported benzyl N-ethyl-N-di-isopropyl ammonium chloride (PSPTC) in principle, the homogeneous reaction is independent of the agitation speed. As shown in (Figure 1), the rate of the reaction increases linearly as the agitation speeds increases from 0 to 300 rpm. Macroscopically, this result indicates that the reaction is carried out in a solid-liquid phase. In fact, the reaction proceeds by accompanying with the dissolving Na₂S in chlorobenzene. The dissolving rate of Na₂S in chlorobenzene is highly influenced by the agitation speed. In general, a high concentration of Na₂S dissolving in organic solvent is obtained at a high agitation speed. Therefore, the conversion of ethyl-2-bromo acetate was increased with the increase in the agitation speed up to 300 rpm. For agitation speeds higher than 300 rpm, the conversion is influenced almost not at all by the agitation speed. The purpose of stirring is to provide a well mixing to dissolve Na₂S in the chlorobenzene in the ethyl-2-bromo acetate presence of PSPTC to form Q₅S. Then, the dissolved Q₅S reacted with to produce ethyl-2-bromoacetate. Therefore, the agitation speed was set at 300 rpm for studying the reaction phenomena from which the resistance of mass transfer stays at a constant value [27-35]. The \(k_{\text{app}}\) values indicate that the mechanical effects brought up by the use of low frequency ultrasonic waves are responsible for the enhancement of the kinetics by harsh mixing, enhancement of mass transfer and in solid-liquid systems, high erosion of the solid particles occurs and consequently the surface area is increased. So, on further, when the same reaction was carried out in conventional method, the observed \(k_{\text{app}}\) value (\(k_{\text{app}}=6.2 \times 10^{-3}\), min⁻¹) almost four fold lesser than in the presence of ultrasound (40 kHz, 300 W, 300 rpm: \(k_{\text{app}}=24.63 \times 10^{-3}\), min⁻¹).

Effect of the amount of newly prepared PSPTC

The experiments were conducted by varying the amount of the newly synthesized polymer-supported benzyl-N-ethyl-N-diisopropylammonium chloride (PSPTC) by keeping other experimental parameters are kept constant. The influence of the amount of PSPTC has been studied by varying the amount of PSPTC from 0.5 g to 2.5 g with respect to ethyl-2-bromo acetate (EBA) under ultrasound irradiation (40 kHz, 300 W). As shown in (Table 1) and (Figure 2), the rate of conversion is increased with increasing in the amount of PSPTC along with ultrasound irradiation (40 kHz, 300 W). The conversion about 75% in the higher concentration of polymer-supported monosite-phase-transfer catalyst in 30 minutes of the reaction. The increase in the \(k_{\text{app}}\) value is attributed to the synergetic effect of ultrasound might be enlarged [36]. The small amount of water can efficiently promote the solubilization of the solid reactant and thus enhance the formation of catalytic intermediate (Q₅S). All the further experiments were done at 1.0 g of catalyst amount.

Effect of the amount of ethyl-2-bromoacetate

To investigate the influence of ethyl-2-bromoacetate (EBA) on the kinetics of synthesis of ethyl-2-bromoacetate under ultrasonic...
Effect of ultrasonic condition the $k_{app}$ value increases with increasing the amount of EBA. When the ethyl-2-bromoacetate concentrations increased, the probability of finding the substrate with active-site of the catalyst and ultrasound enhanced the rate of the reaction [36,37]. It may be due to reduces the surface area between the solid and organic phases, and hence more reactants collide to each other simultaneously we get higher $k_{app}$ value.

**Effect of temperature**

The effect of temperature on the reaction between sodium sulfide and ethyl-2-bromoacetate was studied under otherwise similar conditions. The temperature was varied from 40 to 80°C (Figure 3). The kinetic profile of the reaction is obtained by plotting $-\ln(1-X)$ versus time. It is obvious that the reactivity is increased with an increase in the temperature along with ultrasonic effect [38]. The reason is that the number of reactant molecules which possess higher activation energy at a higher temperature and thus the ultrasonic wave easily passes through the reactor [39,40]. The other point is that the collision of the reactants at higher temperature is also increased. Hence, the apparent rate constant is increased at higher temperature. Arrhenius plots were made in (Figure 4) of $-\ln k_{app}$ against $1/T$ to get activation energy of 53.32 kJ mol$^{-1}$. From the literature survey, the dehydrobromination of (2-bromoethyl) benzene catalyzed by tetroctylammonium bromide (TOAB), an extraction mechanism was proposed [41] due to lower E value (<43 kJ mol$^{-1}$). In general, higher activation energy (more than 43 kJ mol$^{-1}$) suggests an interfacial mechanism [37,42]. The activation energy for the heterogeneous ethylation of phenylacetonitrile was reported to be 63.64 kJ mol$^{-1}$ and for this an interfacial mechanism was proposed [43,44]. Further they concluded that the deprotonation of the substrate takes place at the inter-phase and consequently the organic anion is extracted and reacts in the bulk organic phase. The rate-determining step in the process is the anion exchange at the inter-phase. In our study, the observed E value is 53.32 kJ mol$^{-1}$ (64.66 kJ mol$^{-1}$ under silent condition). Hence, we proposed an interfacial mechanism for our present study [37,46].

**Effect of ultrasonic frequency**

Ultrasonic irradiation is defines as acoustic waves with frequencies in the 20 kHz-100 MHz range [47]. They create cavities generating locally high temperature and pressures [48-51] or strong electric fields [49, 51-53]. Ultrasound is known to accelerate diverse types of organic reactions and it is established generous reactions, which are otherwise slow due to poor mass transfer are accelerated by sonication due to cavitations [50]. It has been reported that a combination of PTC and ultrasound is often better than either of the two techniques alone [51]. In such transfer of species across the interface and ultrasound merely facilitates this transfer, possibly by increasing the interfacial area across which this transfer occurs.

To ascertain the influence of various ultrasonic frequencies on the rate of the reaction with same output power of 300 W, the ultrasonic frequency was varied between 28 and 40 kHz under otherwise similar conditions using PSPTC as the catalyst and also we followed the reaction under silent condition (0 kHz). It has been reported that a combination of PTC and ultrasound is often better than either of the two techniques alone [51]. In such transfer of species across the interface and ultrasound merely facilitates this transfer, possibly by increasing the interfacial area across which this transfer occurs.
Effect of amount of ethyl-2-bromoacetate (EBA), g

<table>
<thead>
<tr>
<th>EBA, g</th>
<th>k_{app} \times 10^2 \text{ min}^{-1} (40 \text{ kHz, } 300 \text{W})</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.25</td>
<td>13.23</td>
</tr>
<tr>
<td>0.5</td>
<td>19.52</td>
</tr>
<tr>
<td>1.0</td>
<td>24.63</td>
</tr>
<tr>
<td>1.5</td>
<td>28.30</td>
</tr>
<tr>
<td>2.0</td>
<td>31.78</td>
</tr>
</tbody>
</table>

Table 2: Effect of the amount of ethyl-2-bromoacetate (EBA) on the rate of synthesis of diethyl-2,2'-thiodiacetate: Na$_2$S (9.25 mmol), ethylbromoacetate (6.35 mmol), 0.2 g biphenyl (internal Standard), chlorobenzene 30 mL, 60°C, PSPTC 1 g, 300 rpm, 40 kHz, 300 W.

Effect of organic solvents

The influence of various organic solvents on the rate of thioetherification of sodium sulfide was followed under otherwise standard reaction conditions. Five organic solvents employed in this study are toluene, anisole, cyclohexane, chlorobenzene, and n-hexane. From the plot of $-\ln(1-X)$ against time, the $k_{app}$ values are obtained. From the (Table 4), chlorobenzene possesses a higher $k_{app}$ value among the five organic solvents, due to its higher dielectric constant. In another view the ultrasonic irradiation can enhance the rate in the presence of more polar solvents due to passing higher ultrasonic waves to the reactor and makes fruitful collision between the reactants, and hence we get higher $k_{app}$ value for chlorobenzene solvent of this system and also this statement is not always true [56-62].

Effect of volume of chlorobenzene

In a homogeneous reaction, the reaction follows the intrinsic kinetic law. The conversion or the reaction rate is directly proportional to the concentration of the reactants in 30 min of reaction. A dilute concentration of the reactant is obtained using a large amount of organic solvent. The conversion of ethyl-2-bromoacetate is increased with the decrease in the volume of chlorobenzene (Table 5). (Figure 5) shows the dependence of the % conversion on the volume of chlorobenzene. The $k_{app}$ value is inversely proportional to the volume of chlorobenzene, as expected.

Effect of different phase-transfer catalysts

Comprehensive comparative kinetic studies for the thioetherification of sodium sulfide by ethyl-2-bromoacetate (EBA) were carried out using 5 mol% of various onium salts viz., polymer-supported benzyl-N-ethyl-N-diisopropylammonium chloride (PSPTC), tetraethylammonium chloride (TEAC), tetrabutylammonium bromide (TBAB), tetrabutylammonium chloride (TBA), benzyltriethylammonium chloride (BTEAC), and benzyldiisopropylammonium chloride (BTEAC). The pseudo-first order rate constant are evaluated for all the catalyst from the plot of $-\ln(1-X)$ versus time and are presented in (Table 6) with ultrasonic condition. The order of the relativities of these quaternary ammonium salts are in decreasing order of their dielectric constant and also this statement is not always true [56-62].

**Table 3**: Influence of the ultrasonic frequencies on the rate of synthesis of diethyl-2,2'-thiodiacetate.

<table>
<thead>
<tr>
<th>Solvents</th>
<th>dielectric constant (ε)</th>
<th>$k_{app} \times 10^2 \text{ min}^{-1}$ (40 kHz, 300W)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Chlorobenzene</td>
<td>5.6</td>
<td>24.63</td>
</tr>
<tr>
<td>Anisole</td>
<td>4.3</td>
<td>21.76</td>
</tr>
<tr>
<td>Toluene</td>
<td>2.4</td>
<td>15.24</td>
</tr>
<tr>
<td>Hexane</td>
<td>2.2</td>
<td>11.52</td>
</tr>
<tr>
<td>Cyclohexane</td>
<td>2.0</td>
<td>9.68</td>
</tr>
</tbody>
</table>

**Table 4**: Influence of organic solvents on the rate of the synthesis of diethyl-2,2'-thiodiacetate: Na$_2$S (9.25 mmol), ethylbromoacetate (6.35 mmol), 0.2 g biphenyl (internal Standard), PSPTC 1 g, 60°C, PSPTC 1 g, 300 rpm, 40 kHz, 300 W.
The critical effect of traces of water on solid-liquid phase transfer reactions has been studied in detail by several groups [4,69-77]. In solid-liquid system, the addition of small amount of water can be useful in forming the catalytic intermediate for conducting intrinsic reactions. The effect of water on this SLPTC was explored under 300 rpm and ultrasonic irradiation (40 kHz, 300 W). (Figure 6) is the plot of conversion versus volume of water (mL) for different amounts of water added, showing that pseudo-first-order kinetic equation can be successfully used to describe the ultrasound assisted-SLPTC system. Without adding water, only 47% of product yield was obtained in 60 minute of reaction; but merely with 1mL of water in the system, the product yield largely increased to 85.3%. Continuing to increase the quantity of water, the reaction rate was increased for further 1mL and then gradually reduced. When the amount of water was added to 30 mL, the solid-liquid system became a liquid–liquid type, and the product yield greatly decreased to 30%, much lower than that in SLPTC. The increase of reaction rate with small amount of water was mainly due to water solubilizing a small part of solid reactant to increase the production of (Q₂⁺)S²⁻ in the inter-phase, thus enhancing the intrinsic reaction rate. When more water was added, the effective concentration of (Q⁺)S²⁻ in the inter-phase would be decreased and the reaction rate was reduced. In the absence of water, the reaction rate of solid reactant and PSPTC in the organic phase was slow, resulting in small product yield 49% after 30 min of reaction. With only 1 mL of water, the formation of (Q⁺)S²⁻ greatly increased and concentrated in the inter-phase and leads to the bulk organic phase where the intrinsic reaction take place.

**Discussion of the Reaction between Sodium Sulfide and Ethyl-2-Bromoacetate**

Known quantities of polymer-supported mono-site phase transfer catalyst (PSPTC) viz., polymer-supported benzyl-N-ethyl-N-diisopropylammonium chloride (PSPTC) (1.0 g), ethyl 2-bromoacetate (1.0 g, 6 mmol) and 0.2 g biphenyl (internal standard in the analysis) in chlorobenzene solvent (30 mL) were added slowly to the mixture of well powdered sodium sulfide (6 g, 77 mmol) in 10 mL water and agitated (300 rpm) in a 250 mL three-necked Pyrex round – bottom batch reactor, which was immersed in a constant temperature (60°C)

![Figure 6: Effect of the amount of water on the synthesis of diethyl-2,2’-thiodiacetate.](image_url)

**Table 5:** Effect of various PTC’s (5mol% based on ethylbromoacetate) on the rate of synthesis of diethyl-2,2’-thiodiacetate: Na₂S (9.25 mmol), ethylbromoacetate (6.35 mmol), 0.2 g biphenyl (internal Standard), chlorobenzene 30 mL, 60°C, PSPTC 1 g, 300 rpm, 40 kHz, 300 W.

<table>
<thead>
<tr>
<th>PTC</th>
<th>kₚ app x 10³, min⁻¹ (40 kHz, 300W)</th>
</tr>
</thead>
<tbody>
<tr>
<td>TBAB</td>
<td>16.86</td>
</tr>
<tr>
<td>TBAC</td>
<td>16.31</td>
</tr>
<tr>
<td>BTEAC</td>
<td>15.58</td>
</tr>
<tr>
<td>TEAB</td>
<td>14.33</td>
</tr>
<tr>
<td>TEAC</td>
<td>13.56</td>
</tr>
</tbody>
</table>

**Figure 5:** Effect of the volume of solvent chlorobenzene on the synthesis of diethyl-2,2’-thiodiacetate: Na₂S (9.25 mmol), ethylbromoacetate (6.35 mmol), 0.2 g biphenyl (internal Standard), chlorobenzene 30 mL, 60°C, PSPTC 1 g, 300 rpm, 40 kHz, 300 W.

**Table 6:** Effect of the volume of chlorobenzene on the rate of synthesis of diethyl-2,2’-thiodiacetate: Na₂S (9.25 mmol), ethylbromoacetate (6.35 mmol), 0.2 g biphenyl (internal Standard), chlorobenzene 30 mL, 60°C, PSPTC 1 g, 300 rpm, 40 kHz, 300 W.

<table>
<thead>
<tr>
<th>Volume of chlorobenzene (mL)</th>
<th>kₚ app x 10³, min⁻¹ (40 kHz, 300W)</th>
</tr>
</thead>
<tbody>
<tr>
<td>30</td>
<td>24.63</td>
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<tr>
<td>40</td>
<td>19.36</td>
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<td>50</td>
<td>15.02</td>
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<tr>
<td>60</td>
<td>12.22</td>
</tr>
<tr>
<td>70</td>
<td>10.56</td>
</tr>
<tr>
<td>80</td>
<td>9.76</td>
</tr>
</tbody>
</table>

The critical effect of traces of water on solid-liquid phase transfer reactions has been studied in detail by several groups [4,69-77]. In solid-liquid system, the addition of small amount of water can be used in forming the catalytic intermediate for conducting intrinsic reactions. The effect of water on this SLPTC was explored under 300 rpm and ultrasonic irradiation (40 kHz, 300 W). (Figure 6) is the plot of conversion versus volume of water (mL) for different amounts of water added, showing that pseudo-first-order kinetic equation can be successfully used to describe the ultrasound assisted-SLPTC system. Without adding water, only 47% of product yield was obtained in 60 minute of reaction; but merely with 1mL of water in the system, the product yield largely increased to 85.3%. Continuing to increase the quantity of water, the reaction rate was increased for further 1mL and then gradually reduced. When the amount of water was added to 30 mL, the solid-liquid system became a liquid–liquid type, and the product yield greatly decreased to 30%, much lower than that in SLPTC. The increase of reaction rate with small amount of water was mainly due to water solubilizing a small part of solid reactant to increase the production of (Q⁺)S⁻ in the inter-phase, thus enhancing the intrinsic reaction rate. When more water was added, the effective concentration of (Q⁺)S⁻ in the inter-phase would be decreased and the reaction rate was reduced. In the absence of water, the reaction rate of solid reactant and PSPTC in the organic phase was slow, resulting in small product yield 49% after 30 min of reaction. With only 1 mL of water, the formation of (Q⁺)S⁻ greatly increased and concentrated in the inter-phase and leads to the bulk organic phase where the intrinsic reaction take place.

**Effect of water**

The critical effect of traces of water on solid-liquid phase transfer reactions has been studied in detail by several groups [4,69-77]. In solid-liquid system, the addition of small amount of water can be used in forming the catalytic intermediate for conducting intrinsic reactions. The effect of water on this SLPTC was explored under 300 rpm and ultrasonic irradiation (40 kHz, 300 W). (Figure 6) is the plot of conversion versus volume of water (mL) for different amounts of water added, showing that pseudo-first-order kinetic equation can be successfully used to describe the ultrasound assisted-SLPTC system. Without adding water, only 47% of product yield was obtained in 60 minute of reaction; but merely with 1mL of water in the system, the product yield largely increased to 85.3%. Continuing to increase the quantity of water, the reaction rate was increased for further 1mL and then gradually reduced. When the amount of water was added to 30 mL, the solid-liquid system became a liquid–liquid type, and the product yield greatly decreased to 30%, much lower than that in SLPTC. The increase of reaction rate with small amount of water was mainly due to water solubilizing a small part of solid reactant to increase the production of (Q⁺)S⁻ in the inter-phase, thus enhancing the intrinsic reaction rate. When more water was added, the effective concentration of (Q⁺)S⁻ in the inter-phase would be decreased and the reaction rate was reduced. In the absence of water, the reaction rate of solid reactant and PSPTC in the organic phase was slow, resulting in small product yield 49% after 30 min of reaction. With only 1 mL of water, the formation of (Q⁺)S⁻ greatly increased and concentrated in the inter-phase and leads to the bulk organic phase where the intrinsic reaction take place.

**Discussion of the Reaction between Sodium Sulfide and Ethyl-2-Bromoacetate**

Known quantities of polymer-supported mono-site phase transfer catalyst (PSPTC) viz., polymer-supported benzyl-N-ethyl-N-diisopropylammonium chloride (PSPTC) (1.0 g), ethyl 2-bromoacetate (1.0 g, 6 mmol) and 0.2 g biphenyl (internal standard in the analysis) in chlorobenzene solvent (30 mL) were added slowly to the mixture of well powdered sodium sulfide (6 g, 77 mmol) in 10 mL water and agitated (300 rpm) in a 250 mL three-necked Pyrex round – bottom batch reactor, which was immersed in a constant temperature (60°C)
ultrasonicator (40 kHz, 300 W). During the reaction, 0.2 mL of the organic sample was withdrawn at the chosen time and diluted into 3 mL of chlorobenzene. The samples analyzed by a gas chromatography (GC-Varian 3700 model). The product viz., (ethyl-2-bromoacetate) was determined from standard curve using biphenyl as an internal standard. In the present solid-liquid system, the mechanism (Scheme 5) is illustrated by the reaction of organic substrate (ethyl-2-bromoacetate, EBA) with the active intermediate Q,S. Without an extra addition of water, the polymer-supported mono-site phase transfer catalyst (QX) diffuses to the surface of the solid particles of Na₂S and converts it into the form of Q,S, which then dissolves in the bulk organic phase.

For the reaction of solid reactant Q,S and organic substrate, ethyl-2-bromoacetate (EBA) catalyzed by the polymer-supported mono-site phase transfer catalyst (QX), the overall reaction is:

\[
QX \text{Na}_2S(S) + EBA_{(org)} \rightarrow (CH_3-CH_2-COOCH_2)_2S_{(org)} + NaCl(S)
\]

Equilibration of KX

The product KX (org) is also in equilibrium with its solid parts and is limited by the solubility in the organic phase:

\[
NaX_{(org)} \leftrightarrow NaX_{(S)}
\]

(i) Reaction of Q,S with benzyl chloride, EBA to form the desired product viz., ethyl-2-bromoacetate, \((CH_3-CH_2-COOCH_2)_2S\) which is represented in the equation (4).

\[
QS_{(org)} + EBA_{(org)} \rightarrow (CH_3-CH_2-COOCH_2)_2S_{(org)} + QCl_{(S)}
\]

Conclusion

In the present study, the rate of the reaction was controlled to study the kinetic aspects of the formation of the ethyl-2-bromoacetate from sodium sulfide and ethyl-2-bromoacetate (EBA) under ultrasonic-PSPTC condition. The apparent reaction rates were observed to obey the pseudo-first order kinetics, performing the reaction in ultrasonic condition resulted in shorter reaction time. The reaction mechanism and the apparent rate constants were obtained from the experimental results, the apparent rate constants are found to be directly dependent on each kinetic variables, viz., (PSPTC), ultrasonic frequency, stirring speed and temperature. However it decreases with increase in the volume of water and volume of chlorobenzene. Energy of activation was calculated from the Arrhenius plot. Based on the experimental evidence, an interfacial mechanism has been proposed. Combination of ultrasound and PSPTC resulted in better
efficacy as compared to the individual operations.

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